

## **TREATMENT OF BATIK EFFLUENT THROUGH COAGULATION-FLOCCULATION PROCESS**

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### **ABSTRACT**

The practice of industry and families disposing of untreated wastewater into the environment without selection has gained popularity, leading to the pollution of our water supplies. This study assesses the efficacy of the coagulation--flocculation technique in treating batik wastewater. Alum was utilized in the coagulation-flocculation treatment of the tie and dye batik effluent samples used in this investigation, which were obtained from a tie and dye fabric manufacturer in Ede at coordinates 7<sup>0</sup> 45' 30" N and 4<sup>0</sup> 26' 19" E. The effectiveness of the treatment method was ascertained by performing physico-chemical and bacteriological studies on the treated and untreated effluent. After treatment, the effluent was determined to be safe when the values from the physico-chemical and bacteriological studies were compared to the Federal Environmental Protection Agency's (FEPA) effluent standard. In the batik effluent, alum decreased the levels of colour, COD (chemical oxygen demand), and TDS (total dissolved solids) by 38.98, 24.46, and 73.91%, respectively. The coagulation--flocculation technique is a highly effective way to clean batik wastewater.

**KEYWORDS:** Batik Effluent, Coagulation, Contaminants, Wastewater, Treatment

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### **1. INTRODUCTION**

In recent times, concerns have arisen over the treatment and disposal of wastewater produced by families and enterprises. This is due to the disturbingly high rate of pollution that emerges from the careless release of untreated wastewater into the environment. Cadmium, Chromium, and Lead are heavy metals found in batik wastewater from batik business outlets, and these levels surpass the necessary environmental quality standards (Slamet et al., 2018). Textile mill wastewater is typically very alkaline, which has a negative impact on aquatic life (Wasif and Chinta, 2008). The process of coagulation-flocculation is a key component of many water and wastewater systems. Actually, because of its affordability and ease of use, the coagulation-flocculation process is one of the most crucial steps in the treatment of water and wastewater. The coagulation-flocculation process is typically incorporated, either as a pre-treatment or post-treatment step, depending on the kind of

treated sample and the overall applicable treatment scheme (Tzoupanos and Zouboulis, 2008). In order to facilitate the formation of larger particles that are easier to remove from the raw water, the coagulant used in the coagulation-flocculation process is meant to neutralize that charge. Although  $\text{FeCl}_3$ ,  $\text{FeSO}_4$ , and other coagulants, such as polyelectrolytes, can be employed, alum [ $\text{Al}_2(\text{SO}_4)_3 \cdot 18\text{H}_2\text{O}$ ] is typically used. When alum is added to water, it hydrolyzes by consuming the alkalinity in the water through processes aided by the aluminum in this salt (Subramanian, 2017). To produce good coagulation, a high-energy, quick mix is required to distribute the coagulant properly and encourage particle collisions. Coagulation is unaffected by excessive mixing, however inadequate mixing will render this stage unfinished. Usually, the rapid-mix chamber has a contact time of one to three minutes (MRWA, 2018). Furthermore, the process of flocculation, a mild step of mixing, aids in the transformation of sub-microscopic micro-floc particles into visible suspended particles. Water or wastewater is prepared for sedimentation once floc reaches its ideal size and strength. The quantity of mix energy and mixing velocity must be carefully considered when designing contact times for flocculation, which can range from 15 to 20 minutes to an hour or longer (MRWA, 2018). Additionally, Badejo et al. (2022) assessed the efficacy of a batch-scale electrocoagulation (EC) technique for treating wastewater rich in indigo dyes and confirmed that the technology may be applied to reduce colour in wastewater rich in indigo dyes used in the textile sector. This study aims to assess the efficacy of the coagulation--flocculation technique in treating batik effluent.

## **2. MATERIALS AND METHODS**

### **2.1 Materials and Equipment Required for the Study**

Aluminum sulphate (Alum), Flocculating machine, Jar test apparatus, GPS, Samples of tie and dye (batik) effluent, Standard laboratory equipment for physico-chemical and bacteriological tests are among the supplies and tools used in this research project.

### **2.2 Methods**

#### **Preparation of alum (coagulant)**

An alum solution was made by dissolving 200g of aluminum sulphate (alum) in 1000ml of distilled water. The alum was obtained from a store in Osogbo, Nigeria.

### **Collection of effluent samples**

Batik effluent samples were collected from a tie and dye fabric manufacturer in Ede, Nigeria, located at coordinates 7° 42' 25'' N and 4° 23' 38'' E).

### **Jar test on the effluent sample**

The effluent sample underwent a jar test in accordance with the protocol described by Familusi et al. (2021).

### **Coagulation of the batik effluent**

The alum dose (found from the jar test) was added to 0.001m<sup>3</sup> of the batik effluent in the flocculation bucket, which had a known volume of batik effluent delivered into the coagulation/flocculation bucket. After inserting the flocculation bucket into the flocculating machine, the samples were vigorously mixed for five minutes by the roller, and then slowly mixed for fifteen minutes. After an hour of settling, the sample was decanted.

### **Physico-chemical and bacteriological analyses**

Osun State Water Corporation, Ede, Nigeria received three samples of each of the treated (coagulated) and untreated (batik) effluent for physico-chemical and bacteriological studies. The parameters were established in accordance with the American Public Health Association's recommended standard procedures for the examination of water and wastewater (APHA, 1998).

## **3. RESULTS AND DISCUSSION**

### **3.1 Jar Examination**

The findings of the jar test showed that 295 millilitres of coagulant (alum) were needed to treat 500 millilitres of batik effluent.

### **3.2 Physico-Chemical and Bacteriological Parameters**

The following are the physico-chemical and bacteriological characteristics of the treated and untreated wastewater samples. Equation 1 was used to calculate the efficiency of the coagulation-flocculation process.

$$\eta = \frac{(C_1 - C_2) \times 100}{C_1} \quad (1)$$

where  $\eta$  is the efficiency of the treatment unit,

$C_1$  is the parameter value before treatment, and

$C_2$  is the parameter value after treatment.

## **pH**

After the batik effluent was coagulated with alum, the pH value increased to  $5.100 \pm 0.044$  from  $5.490 \pm 0.036$ . The pH increases somewhat throughout the coagulation process, however the result met the limit (6–9) set forth in the FEPA effluent regulations (1991). Alum often operates in an alkaline setting. According to Carrizales et al. (2021), effluent that is to be dumped into aquatic bodies should typically have a pH of 6.5 to 8.5. The treated sample somewhat failed to meet this criteria. It was discovered that the therapy effectively lowered the pH by 7.14%.

## **Turbidity**

After coagulating with alum, the batik effluent's turbidity value, which was  $500.000 \pm 1.136$  FTU, increased to  $484.000 \pm 1.732$  FTU. The waxing procedure, which left behind leftover wax, and the leftover colouring water, which contained suspended dyes, are the causes of the high turbidity in batik wastewater (Soedjono et al., 2021). It was discovered that the treatment method was 3.2% effective in eliminating turbidity

## **Temperature**

After coagulating with alum, the temperature of the batik effluent was measured at  $25.420 \pm 0.171$  °C, and it was found to be  $26.000 \pm 0.361$  °C. The results met the 40 °C limitations promulgated by the effluent standards of FEPA (1991). The temperature dropped by -2.282 percent, however the treated and untreated wastewater do not differ significantly in temperature.

## **Colour**

The batik effluent's colour was measured at  $2950.000 \pm 27.839$  HU. After coagulating with alum, the colour value decreased to  $1800.000 \pm 7.000$  HU, indicating a 38.983 % coagulation effectiveness in the effluent's colour removal.

## **Conductivity**

After coagulating with alum, the conductivity of the batik effluent was measured at  $2500.000 \pm 5.196$   $\mu\text{S}/\text{cm}$ ; this value was reduced to  $2200.000 \pm 7.000$   $\mu\text{S}/\text{cm}$ . Since conductivity in a water or wastewater sample is a function of TDS, the decrease in conductivity level may be linked to the decrease in TDS observed during coagulation. Additionally, this aligns with the findings of Carrizales *et al.* (2021). It was discovered that the coagulation efficiency was 12 %.

## **Total Suspended Solids (TSS)**

After coagulating with alum, the batik effluent's TSS value decreased to  $1.900 \pm 0.046$  mg/l from  $4.688 \pm 0.013$  mg/l. The readings obtained met the effluent regulations of the Federal Environmental Protection Agency (1991) limit of 30 mg/l. It was discovered that the treatment process had an efficiency of 59.571 %.

## **Total Dissolved Solids (TDS)**

After coagulating with alum, the batik effluent's TDS value decreased to  $274.000 \pm 1.732$  mg/l from  $1050.000 \pm 5.220$  mg/l. The readings obtained met the effluent regulations of the Federal Environmental Protection Agency (1991) limit of 2000 mg/l. This aligns with the research conducted by Carrizales *et al.* (2021). It was discovered that the treatment method had an efficiency of 73.905 %.

## **Alkalinity**

After coagulating with alum, the batik effluent's total alkalinity value—which was  $126.000 \pm 3.279$  mg/l—was reduced to  $122.000 \pm 1.054$  mg/l. The carbonates produced during the coagulation process may be the cause of the wastewater's increased alkalinity level. The treatment method was determined to have an efficiency of 3.175 %.

### **Hardness**

After coagulating with alum, the batik effluent's total hardness value increased to  $144.000 \pm 0.346$  mg/l from  $126.000 \pm 2.291$  mg/l. It was discovered that the efficiency of the treatment process was 14.286 %.

### **Silica**

After coagulating with alum, the batik effluent's silica content decreased to  $24.000 \pm 0.265$  mg/l from  $27.290 \pm 0.185$  mg/l. Because alum has a substantial silica concentration, the wastewater's greater silica level following alum coagulation may be explained by this. It was discovered that the treatment method had an efficiency of 12.056 %.

### **Sulphate**

After coagulating with alum, the batik effluent's sulphate content decreased to  $128.000 \pm 0.436$  mg/l from  $135.000 \pm 0.265$  mg/l. Alum had a removal effectiveness of just 5.15 % for Sulphate, and the values obtained were in compliance with the FEPA (1991) effluent guidelines, which set a limit of 500 mg/l.

### **Chloride**

After coagulating with alum, the batik effluent's chloride content decreased to  $83.000 \pm 0.361$  mg/l from  $90.000 \pm 0.866$  mg/l. The readings obtained satisfied the limit (600 mg/l) imposed by the effluent standards of FEPA (1991). It was discovered that the treatment method had a 7.778 % removal effectiveness for chloride.

### **Manganese**

After coagulating with alum, the value of the manganese in the batik effluent was  $3.104 \pm 0.007$  mg/l, compared to the initial value of  $3.461 \pm 0.010$  mg/l. It was discovered that the treatment method removed manganese with an efficiency of 10.315 %.

## **Zinc**

After coagulating with alum, the zinc value of the batik effluent was  $12.463 \pm 0.033$  mg/l, and it was  $10.592 \pm 0.007$  mg/l after that. The results meet the effluent guidelines of FEPA (1991) limit of less than one milligram per litre. It was discovered that the treatment method's zinc removal effectiveness was 15.012 %

## **Aluminium**

After alum was added to the batik effluent, the aluminum content decreased to  $6.314 \pm 0.013$  mg/l from  $8.591 \pm 0.037$  mg/l. It was discovered that the treatment technique had a 2.277 % removal effectiveness for aluminium.

## **Chromium**

After coagulating with alum, the value of the batik effluent's chromium decreased to  $1.9470 \pm 0.003$  mg/l from  $2.169 \pm 0.002$  mg/l. The results met the  $<1$  mg/l criteria set forth in the effluent regulations of FEPA (1991). It was discovered that the treatment method had 10.25% removal effectiveness for chromium.

## **Iron**

The iron content of the batik effluent was  $54.360 \pm 0.314$  mg/l; however, after alum was added, the value dropped to  $38.000 \pm 0.529$  mg/l. The value attained following treatment meets the  $<1$  mg/l restrictions set forth in the effluent regulations of FEPA (1991). It was discovered that the treatment method had 30.096 % iron removal efficiency.

## **Nitrate**

After coagulating with alum, the batik effluent's nitrate value decreased to  $14.823 \pm 0.025$  mg/l from  $15.974 \pm 0.601$  mg/l. The readings obtained meet the 20 mg/l maximum limitations set forth in the effluent regulations of FEPA (1991). It was discovered that the treatment method was 7.206 percent effective in eliminating nitrate.

### **Bio-Chemical Oxygen Demand (BOD)**

The batik effluent's BOD value was  $0.100 \pm 0.017$  mg/l; however, after alum coagulation, the value increased to  $0.200 \pm 0.017$  mg/l. The results meet the 30 mg/l limit set forth in the effluent standard of FEPA (1991). It was discovered that the treatment method's BOD removal efficiency was -100 %.

### **Chemical Oxygen Demand (COD)**

After the batik effluent was coagulated with alum, the COD value increased to  $420.000 \pm 3.775$  mg/l from  $556.000 \pm 1.732$  mg/l. The COD in the wastewater was reduced by 24.60% thanks to the coagulation process.

### **Coliform**

After coagulating with alum, the value of the batik effluent's coliform dropped to 160 MPN/100 ml from 180+ MPN. Coliform indicates that harmful microorganisms may have been present in the wastewater sample. The levels attained met the 400 MPN/100 ml limit set forth in the effluent regulations of FEPA (1991).

## **4. CONCLUSION**

The coagulation-flocculation method of treating batik effluent has shown to be effective in lowering the pollutant level of a variety of wastewater parameters. In the batik effluent, the method specifically decreased the levels of colour, chemical oxygen demand (COD), and total dissolved solids (TDS) by 38.98, 24.46, and 73.91 %, respectively. Nevertheless, the effluent's total hardness and BOD contaminant levels increased as a result of the coagulation-flocculation process. Although the procedure has not been very useful in treating wastewater, due to its efficiency, it is hereby suggested for treatment of wastewater in homes, businesses, and communities.

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